## California Environmental Protection Agency

# Air Resources Board

**Vapor Recovery Test Procedure** 

**TP - 201.20** 

Pressure Integrity of Drop Tube Overfill Protection Devices

Adopted: February 1, 2001

Note: This procedure is being adopted. Because all the text is affected, for ease of viewing, the underline is omitted as allowed by title 1, California Code of Regulations, section 8.

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## Pressure Integrity of Drop Tube Overfill Protection Devices

Definitions common to all certification and test procedures are in:

#### **D-200 Definitions for Vapor Recovery Procedures**

For the purpose of this procedure, the term "CARB" refers to the State of California Air Resources Board, and the term "Executive Officer" refers to the CARB Executive Officer, or his or her authorized representative or designate.

#### 1. PURPOSE AND APPLICABILITY

1.1 The purpose of this procedure is to quantify the pressure integrity of overfill protection devices located in the Phase I product drop tube on two-point Phase I systems. It is applicable only to those Gasoline Dispensing Facilities (GDF) equipped with an overfill protection device located in the Phase I product drop tube. This procedure determines compliance with the performance standard for the maximum allowable leakrate as defined in the Certification Procedure (CP-201).

#### 2. PRINCIPLE AND SUMMARY OF TEST PROCEDURE

- 2.1 A compatible product cap is modified to allow the introduction of nitrogen into the Phase I drop tube. A pressure-measuring device is connected to the modified cap. If the resulting measured nitrogen flowrate necessary to maintain a steady-state pressure of 2.00 inches H<sub>2</sub>O is less than, or equal to, the maximum allowable leakrate the overfill protection device is verified to be in compliance.
- 2.2 If the introduction of nitrogen, at a flowrate equal to the maximum allowable leakrate, does not result in a steady state pressure that meets, or exceeds, the value specified in CP-201, the Phase I product adaptor is inspected and tested. Any leaks attributable to the Phase I product adaptor are corrected and the test is repeated to ensure the measured pressure versus flowrate is attributable only to the overfill protection device.

#### 3. BIASES AND INTERFERENCES

- 3.1 Missing or defective gaskets on the Phase I product adaptor, or a loose adaptor, may bias the results towards noncompliance. This bias is eliminated by testing the Phase I product adaptor for leaks prior to final determination of the compliance status of the overfill protection device.
- **3.2** Vehicle refueling during the test may bias the results. No vehicle refueling or bulk deliveries to any of the tanks at the facility shall occur during this test
- **3.3** Product levels less than four (4) inches above the highest opening at the bottom of the submerged drop tube may bias the test toward noncompliance.
- 3.4 Liquid levels in the drop tube that are above the location of the overfill protection device will bias the results toward compliance. Ensure that the liquid level is below the overfill protection device.
- **3.5** Leaks in the test equipment will bias the results toward noncompliance. Prior to conducting the test, this bias is eliminated by conducting a leak check of the test equipment. During the test, this bias is eliminated by using leak detection solution to verify the absence of leaks in the test equipment.

#### 4. SENSITIVITY, RANGE, AND PRECISION

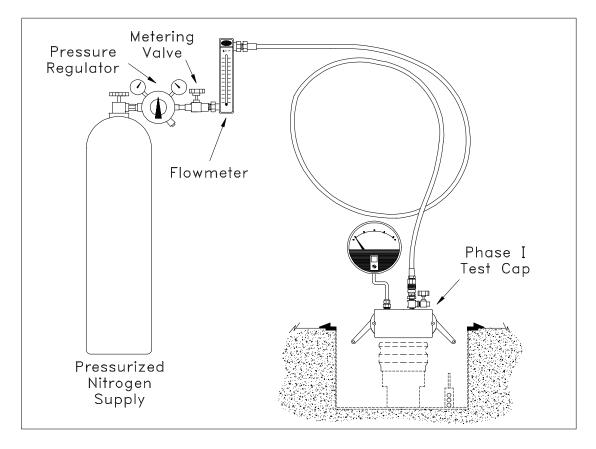
- **4.1** The measurable leakrates are dependent upon the range of the flowmeter used for the test. The recommended flowmeter range specified in Section 5.1 provides sufficient precision at the maximum allowable leakrate defined in CP-201.
- **4.2** The sensitivity of the pressure measuring device is 0.01 inches  $H_2O$  for electronic pressure measuring devices and 0.05 inches  $H_2O$  for mechanical pressure gauges.5.

#### **EQUIPMENT**

- 5.1 Drop Tube Pressure Integrity Assembly. Use a product cap compatible with the Phase I product adaptor. The cap shall be equipped with a pressure tap and a flowmeter capable of measuring flowrates equal to the maximum allowable leakrate specified in CP-201 and three times the maximum allowable leakrate. The maximum allowable full-scale range for the flowmeter shall be 1.0 CFH. The flowmeter shall be calibrated for use with nitrogen. An example of a complete Drop Tube Pressure Integrity Assembly is shown in Figure 1. An example of a Product Cap Test Assembly is shown in Figure 2.
- **5.2** Pressure Measuring Device. Use a pressure-measuring device to monitor the pressure in the drop tube.
  - **5.2.1** If an electronic pressure-measuring device is used, the maximum fullscale range of the device shall be 10 inches  $H_2O$ . The minimum accuracy shall be 0.5 percent and the pressure measuring device shall be readable to the nearest 0.01 inches  $H_2O$ .

**5.2.2** If a mechanical pressure-measuring device is used, the maximum fullscale range shall be 5 inches H<sub>2</sub>O. The minimum accuracy shall be 1.0 percent and the minimum graduations shall be 0.05 inches H<sub>2</sub>O. The minimum diameter of the pressure gauge face shall be 4 inches.

Figure 1
Drop Tube Pressure Integrity Assembly



- **5.3** Nitrogen. Use commercial grade gaseous nitrogen in a high-pressure cylinder, equipped with a two-stage pressure regulator and a one psig pressure relief valve.
- **5.4** Stopwatch. Use a stopwatch accurate to within 0.2 seconds to time the duration of the test.
- **5.5** Leak Detection Solution. Any commercial liquid solution designed to detect vapor leaks may be used to verify the pressure integrity of the Phase I product adaptor during this test.
- **5.6** Vapor Poppet Pressure Relief Assembly. Use an assembly to open the Phase I vapor poppet during the test. This will ensure that the pressure on the underground storage

- tank (UST) side of the overfill protection device is at zero gauge. An example of a Vapor Poppet Pressure Relief Assembly is shown in Figure 3.
- **5.7** Traffic Cones. Use traffic cones to encircle the area containing the Phase I manholes while the test is being conducted.
- 5.8 Tank Gauging Stick. Use a tank gauging stick of sufficient length to verify that the UST liquid level is at least four (4) inches above the highest opening at the bottom of the submerged drop tube. The tank gauging stick shall be equipped with a non-sparking "L" bracket at the end.

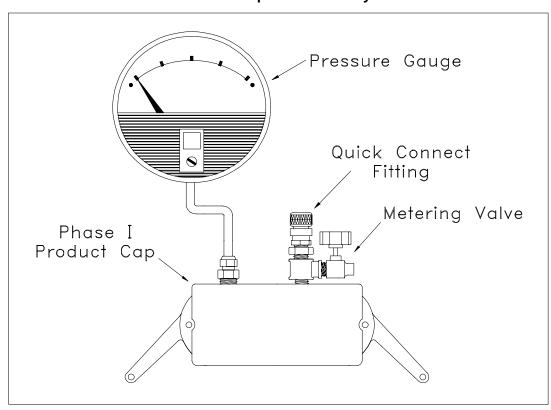


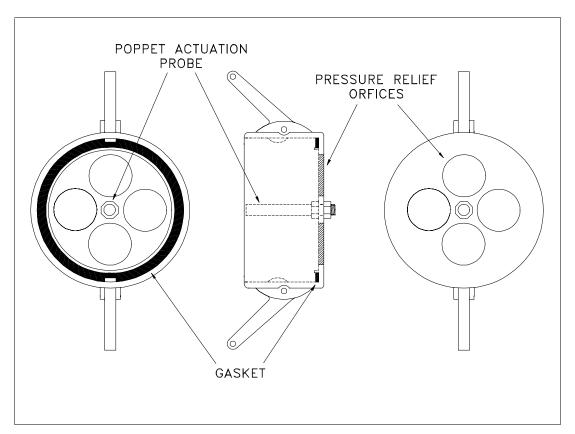
Figure 2
Product Cap Test Assembly

#### 6. PRE-TEST PROCEDURES

6.1 The flowmeter and pressure-measuring device shall be calibrated within the 180 days prior to conducting the test. The flowmeter(s) shall be calibrated for use with nitrogen. Calibrations shall be conducted in accordance with EPA or CARB protocols. CARB calibration methodology for flowmeters are contained in Appendix D of Air Monitoring Quality Assurance, Volume VI, Standard Operating Procedures for Stationary Source Emission Monitoring and Testing, January 1979.

- **6.2** Place the traffic cones around the perimeter of the Phase I containment boxes, allowing sufficient space to safely conduct the test.
- **6.3** Remove the lids of the Phase I containment boxes. Visually determine that the drop tube is equipped with an overfill protection device. If the drop tube is not equipped with an overfill protection device, the test will only quantify leaks that occur at the Phase I adaptor.
- **6.4** Inspect the Phase I product adaptor to ensure that the gasket is intact and that the adaptor is securely attached to the Phase I product stem.
- **6.5** Verify that the liquid level in the storage tank is at least four (4) inches above the highest opening at the bottom of the submerged drop tube. This may be accomplished by using a tank gauging stick equipped with a non-sparking "L" bracket on the end.

Figure 3
Vapor Poppet Pressure Relief Assembly



#### 7. TEST PROCEDURE

7.1 Connect the Drop Tube Pressure Integrity Assembly to the Phase I product drop tube as

- shown in Figure 1. Connect the nitrogen supply line to the inlet of the flowmeter.
- **7.2** Connect the Vapor Poppet Pressure Relief Assembly to the Phase I vapor poppet to bring the UST headspace to atmospheric pressure.
- 7.3 With no vehicle refueling occurring, open the nitrogen supply and adjust the nitrogen flowrate to at least three times the maximum allowable leakrate specified in CP-201, and start the stopwatch. Use leak detection solution on the Drop Tube Pressure Integrity Assembly and verify that the test equipment does not leak at any of the connections.
- **7.4** Wait until the pressure measuring device records a pressure between 2.00 and 2.20 inches H<sub>2</sub>O.
  - 7.4.1 If the pressure does not reach at least 2.00 inches H<sub>2</sub>O within 90 seconds, the Drop Tube assembly does not comply with the maximum allowable leakrate.
  - 7.4.2 If the pressure reaches at least 2.00 inches H<sub>2</sub>O, reduce the introduction of nitrogen to the allowable leakrate specified in CP-201. Wait until the pressure reaches steady state conditions for at least ten (10) seconds and record both the nitrogen flowrate and the steady state pressure. If the steady state pressure is less than 2.00 inches H<sub>2</sub>O, the Drop Tube assembly does not comply with the maximum allowable leakrate.

#### 8. POST-TEST PROCEDURES

- **8.1** Carefully remove the Drop Tube Pressure Integrity Assembly and the Vapor Poppet Pressure Relief Assembly from the Phase I connections. Replace the caps on the appropriate Phase I adaptors, and the appropriate lids on the containment boxes.
- **8.2** Remove the traffic cones from the Phase I area.
- **8.3** If the steady-state pressure, at a nitrogen introduction rate equal to the allowable leakrate, was not equal to 2.00 inches  $H_2O$ , use Equation 9-1 to determine the leakrate at 2.00 inches  $H_2O$ .

#### 9. CALCULATING RESULTS

**9.1** If the flowrate of Nitrogen was at the upper limit of the flowmeter and the measured pressure never reached 2.00 inches H<sub>2</sub>0, but was greater than 0.0 inches H<sub>2</sub>O, the actual leakrate at a pressure of 2.00 inches H<sub>2</sub>O shall be calculated as follows:

$$Q_{2.00} = (2.00)^{1/2} \left[ \frac{Q_{actual}}{(P_{actual})^{1/2}} \right]$$
 Equation 9 – 1

Where:

 $Q_{2.00}$  = The leakrate of the drop tube assembly at 2.00 inches  $H_2O$ , cubic feet per hour

Q<sub>actual</sub> = The actual introduction rate of nitrogen, cubic feet per hour

Pactual = The actual measured steady-state pressure at Qactual, inches H2O

2.00 = Pressure, inches  $H_2O$ 

#### 10. REPORTING RESULTS

**10.1** Report the results of the quantification of the leakrate through the drop tube overfill protection assembly as shown in Form 1.

#### 11. ALTERNATE PROCEDURES

11.1 This procedure shall be conducted as specified. Modifications to this test procedure shall not be used to determine compliance unless prior written approval has been obtained from the ARB Executive Officer, pursuant to Section 14 of Certification Procedure CP-201.

# Form 1 Field Data Sheet Drop Tube Overfill Protection

Facility: Test Date:		Test Date:	Tester(s):		Tester(s):		
Address:			City:			Zipcode:	
Make & Model of Overfill Protection:				Phase II System Type:			
Date of Last Flowmeter Calibration:				Date of Last Pressure Device Calibration:			
Test Results							
Product Grade	Nitrogen Flowrate, CFH		Pressure, Inches H <sub>2</sub> O		hes H₂O	Make & Model of Overfill Protection	
Comments:							